

DOCKET NO: 268510US0PCT

IN THE UNITED STATES PATENT & TRADEMARK OFFICE

IN RE APPLICATION OF :
BERND ZASCHKE, ET AL. : EXAMINER: COONEY, J.
SERIAL NO: 10/530,707 :
FILED: APRIL 8, 2005 : GROUP ART UNIT: 1711
FOR: METHOD FOR PRODUCING RIGID :
POLYURETHANE FOAMS BY MEANS
OF GRAFT POLYHYDRIC ALCOHOLS

APPEAL BRIEF

SIR:

The following is an appeal of the examiner's final rejection of December 7, 2007 of claims 1-15 and 17-19 as anticipated and/or obvious. A Notice of Appeal along with a petition for a one-month extension of time was filed on January 4, 2008. A petition for a one-month extension of time for filing this brief is filed herewith.

(i) Real Party In Interest

The real party in interest is BASF Aktiengesellschaft, now, BASF SE, by assignment recorded at reel/frame 016486/0992-0994.

(ii) Related Appeals And Interferences

Appellants, appellants' legal representative and the assignee are not aware of any related appeals and interferences which will directly affect or be directly affected, or have a bearing on the Board's decision in the pending appeal. Any copies of decisions rendered by a court or the Board, if any, in any proceeding identified would be attached as related proceedings

appendix (x).

(iii) Status Of Claims

Appellants' state the status of all the claims in the proceeding as follows:

Claims 1-15 and 17-19 are rejected and active in this application and are herein appealed.

No claims have been identified as allowed or confirmed.

No claims have been identified as withdrawn.

No claims have been identified as objected to.

Claim 16 has been canceled.

(iv) Status Of Amendments

No amendments have been filed subsequent to final rejection. A statement as to status is not applicable.

A copy of the claims herein appealed, is attached as appendix (viii).

(v) Summary Of Claimed Subject Matter

The claimed invention is directed to a process for producing closed-celled rigid polyurethane foams by reacting (page 2, lines 34-35 and page 3, lines 7-8)

- a) crude MDI having an NCO content of from 29 to 33% by weight and a viscosity at 25°C in the range from 150 to 1000 mPa•s with (column 8, lines 33-36)

- b) compounds having at least two hydrogen atoms reactive toward isocyanate groups, in the presence of (page 2, lines 39-40)
- c) catalysts, and (page 2, line 42)
- d) blowing agents, (page 2, line 44)

which comprises the presence, among the compounds having at least two hydrogen atoms reactive toward isocyanate groups, of at least one graft polyol (page 3, lines 1-3), wherein said closed-celled rigid polyurethane has a proportion of closed cells in the foam of at least 88% (page 3, lines 7-10).

The claimed invention also directed to a graft polyol comprising polymerized ethylenically unsaturated monomers in polyether alcohols having a hydroxy value in the range from 100 to 600 mg KOH/g, obtained by an addition reaction of alkylene oxides onto H-functional starter substances, the starter substances having been selected from the group consisting of polyfunctional alcohols, sugar alcohols, aliphatic amines, and aromatic amines (page 6, lines 17-31 and claim 13 as originally presented).

Rigid polyurethane foams having a closed-cell structure are known for thermal insulation. Reduced molding times and good mold flow properties are still sought in closed-celled rigid polyurethane foam producing processes.

The claimed invention addresses this problem by providing a process for preparing rigid closed-cell polyurethane foam having **a proportion of closed cells of at least 88%** comprising reacting MDI having **an NCO content of from 29-33% and specified viscosity** with a compound having at least two reactive hydrogen atoms comprising comprises at least

one graft polyol in the presence of catalyst and a blowing agent. Appellants have discovered that a graft polyol provides for good properties in the process for producing a closed-celled rigid polyurethane foam. Such a process or graft polyol are nowhere disclosed or suggested in the cited art of record.

No means plus function or step plus function as permitted by 35 U.S.C. 112, sixth paragraph are used and therefore none are identified.

(vi) Grounds Of Rejection To Be Reviewed On Appeal

1) The rejection of claims 1-6, 12, 13 and 17-19 under 35 U.S.C. § 102(b) over Heyman et al. U.S. 5,919,972 is presented for review.

2) The rejection of claims 7-11 and 14-15 under 35 U.S.C. § 103(a) over Heyman et al. U.S. 5,919,972 in view of EP 786,480 and Isobe et al. U.S. 6,433,033 is presented for review.

3) The rejection of claims 13 and 19 under 35 U.S.C. § 102(b) over Perry et al. U.S. 6,127,443 is presented for review.

4) The rejection of claims 14-15 under 35 U.S.C. § 103(a) over Perry et al. U.S. 6,127,443 in further view of Isobe et al. U.S. 6,433,033 is presented for review.

(vii) Arguments

The rejections of claims 1-6, 12, 13 and 17-19 under 35 U.S.C. § 102(b) over Heyman et al. U.S. 5,919,972 and of claims 7-11 and 14-15 under 35 U.S.C. § 103(a) over Heyman et al. U.S. 5,919,972 in view of EP 786,480 and Isobe et al. U.S. 6,433,033

Claims 1-12 and 17-18

This embodiment of the claimed invention is directed to a process for producing a closed-celled rigid polyurethane and a rigid polyurethane foam.

The examiner has committed reversible error in concluding the claimed invention to be both anticipated and obvious over the cited references as none of the cited art of record discloses or suggests the claimed at least 88% closed cell structure or the claimed crude MDI NCO content of 29 to 33% or viscosity of 150 to 1000 mPa.s.

Heyman et al. fails to disclose or suggest the claimed process of producing a **closed-cell** rigid polyurethane foam having a **proportion of closed cells of at least 88%**.

Heyman et al. describes an **open cell foam** and therefore fails to describe a closed-celled rigid polyurethane foam having a proportion of closed cells of at least 88%.

The evidence of the disclosure of an open cell foam is as follows:

Heyman et al. describes a water blown molded polyurethane foam which exhibits little or no shrinkage.

“Water blown molded polyurethane foams prepared with this graft polymer dispersion exhibit **little or no shrinkage**.” (column 1, lines 15-17).

“Molded polyurethane foams manufactured from this graft polymer dispersion are dimensionally stable and exhibit **little or no shrinkage**.” (column 1, lines 60-62).

The reference describes the known use of low activity surfactants to reduce foam shrinkage.

“The various attempts made to **reduce foam shrinkage** included using **low activity surfactants**, reducing the amount of ethylene oxide termination on the polyether polyol to slow its reactivity, or using a graft polymer dispersion prepared by the continuous process rather than by the semi-batch process.”(column 1, lines 26-27)

A surface active agent is used in order to achieve the goal of a high grade polyurethane.

“A surface-active agent is generally **necessary for production of high grade polyurethane** foam according to the present invention, since in the absence of same, the foams collapse or contain very large uneven cells.”(column 10, lines 18-21)

Accordingly, Heyman et al. is directed to a polyurethane having low shrinkage and incorporates a surfactant in order to prevent foam collapse and to have even cells.

However, the procedures practice by Heyman et al. are used to provide a polyurethane foam having **an open cell structure**. An open cell structure is evidenced by the disclosure of Gallagher U.S. 5,208,271 which reports the reduction or elimination of foam shrinkage by addition of a surfactant which **opens cells** in the foam, a result which previously necessitated mechanical crushing.

“The **elimination of foam shrinkage by opening the cells** using new types of surfactants was the topic of a paper by D. R. Battice, et al., New Cell Opening Surfactants For Molded High Resiliency Polyurethane Foam, 30th Annual Polyurethane Technical Marketing Conference, Oct. 15-17, 1986, pp. 145-148. The new **surfactants that promoted good cell drainage and eliminated foam shrinkage** were identified as X2-5249 and X2-5256, both silicone-based and manufactured at the time by Dow Corning. These surfactants successfully reduced foam shrinkage over a previous Dow Corning® 5043 surfactant.” (column 1, lines 24-35)

“It has been found that perfluoro sulfonamide surfactants used in the invention **prevent shrinkage** of molded flexible polyurethane foams, **avoiding the necessity for mechanical crushing**, and provide suitable alternatives to silicone-based surfactants.” (column 1, line 67 through column 2, line 3)

“To obtain a flexible foam adequately stabilized against collapse and having a good closed-cell structure, it is known to add a surfactant. A flexible foam having a **high number of closed cells, however, leads to shrinkage**. One means generally employed to open the cells and **eliminate foam shrinkage is to mechanically treat the foam by**

crushing with rollers, with a vacuum technique, or by lancing. It would be desirable, however, to produce a surfactant that stabilizes the foam against collapse while **opening the cells of the foam without the necessity for mechanical treatment.**" (column 1, lines 13-23)

Thus, in this area of technology, addition of a surfactant will prevent shrinkage by **opening the cell structure**, without the need for crushing. It is also known that a high number of closed cells produces a foam subject to shrinkage.

Accordingly, since Heyman et al. is directed to a shrinkage reduce polyurethane foam and **adds a surfactant**, which was found to be necessary to produce such a foam, it is clear that the foam of Heyman et al. has a predominantly open cell structure and does not have **at least 88% closed cells**.

While the official action asserts a closed cell structure is inherent to Heyman et al. appellants have provided evidence to the contrary.

Further, appellants have previously noted the physical characterization appearing in Table 2, at column 12 of Heyman et al. which describes air flow properties of 0.63-2.08, air flow being a property which can only be measured for foams having predominately open cells as closed cells prevent an air flow through the foam. While the examiner has noted that the air flow measurements are measured after crushing, leading the examiner to the conclusion that the reference is directed to a closed cell foam, the further characterization of the reference of "low shrinkage" leads to the contrary conclusion. If the foam of Heyman et al. were of a closed cell proportion of at least 88%, the foam of Heyman et al. would not perform as a low shrinkage foam. Samples 2 and 3 in Table 2, **inventive samples** according to Heyman et al. exhibited

shrinkage distances of only 2/0 and 0/0 mm, clearly identifying these foams as low shrinkage.

The absence of significant shrinkage is evidence that the Heyman et al foams do not have a closed cell proportion of at least 88%.

In contrast the claimed invention is directed to a process for producing **closed-celled** rigid polyurethane foams having a proportion of closed cells of at least 88%. Such foams are useful for thermal insulation and for construction and have fundamentally different properties from those of the foam of Heyman et al.

Notwithstanding the failure of Heyman et al. to describe a foam having a closed cell content of at least 88%, the reference fails to disclose a further claimed aspect of the invention as follows:

Heyman Et Al. Fail To Describe An MDI Having And NCO Content Of 29-33% And A Viscosity Of 150 To 1000 mPa·S

The official action, on page 2, asserts that based on the materials employed in the making of the foams of Heyman et al. **it is held** that the disclosure is inherently concerned with formation of articles that are closed celled to the degree claimed by applicants.

However, Heyman et al. never describes an MDI having an NCO content of 29-33% and a viscosity of 150 to 1000 mPa·s. Column 9, lines 5-30 of Heyman et al. describes the polyisocyanate component but nowhere describes the claim limitations of an NCO content of 29-33% and a viscosity of 150 to 1000 mPa·s. In the absence of a disclosure of this claim limitation the claimed process is clearly not rendered obvious by this reference.

There is no evidence to support the examiner's assertion that the claimed isocyanate component is inherent to Heyman et al.

As Heyman et al. fails to disclose or suggest a closed-celled rigid polyurethane foam having a proportion of closed cells of at least 88% producing process nor a polyisocyanate component having an NCO content of 29-33% and a viscosity of 150 to 1000 mPa·s, the claimed invention is clearly neither anticipated nor rendered obvious from this reference. The decision of the examiner must be reversed.

The basic deficiencies of the primary reference are not cured by either of the secondary references, as neither describes a closed-celled rigid polyurethane foam.

EP 786,480 merely describes the preparation of a polymer polyol which may be used in the generic production of polyurethane articles such as a polyurethane foam, but there is no disclosure or suggestion of a closed-celled rigid polyurethane foam.

Claims 7 and 8

Further, while EP '480 has been cited for a disclosure of a narrow particle size distribution, claim 7 recites a distribution of from 0.1 to 8 μm while claim 8 recites a bimodal distribution. EP '480 describes a narrow particle size distribution ranging from 0.5 to 2.5 microns (see abstract). Thus, the reference identifies a range of only 2 microns as narrow. Such a narrow distribution does not render obvious the particle size distribution of claim 7 which is 7.9 microns wide, nor a bimodal particle size distribution which is nearly the antithesis of "narrow." Thus, while EP '490 has been cited for appellants' particle size distribution, the

reference can not render obvious either of claims 7 or 8 and accordingly claims 7 and 8 are separately patentable for failing to suggest the claimed particle size distributions.

Isobe et al. is directed to the production of a high-durability **flexible** polyurethane cold cure molded foam (see Abstract) and therefore is not directed to a closed-celled **rigid** polyurethane foam. As these secondary references fail to disclose or suggest a closed-celled rigid polyurethane foam, the basic deficiencies of the primary reference are not cured and accordingly the claimed invention is clearly not obvious from this combination of references.

In view of the examiner's errors the examiner's decision must be reversed.

The Rejection Of Claims 13 And 19 Under 35 U.S.C. § 102(B) Over Perry Et Al. U.S. 6,127,443 And Of Claims 14-15 Under 35 U.S.C. § 103(A) Over Perry Et Al. U.S. 6,127,443 In Further View Of Isobe Et Al. U.S. 6,433,033

Claims 13-15 and 19

This embodiment of the claimed inventions is directed to a graft polyol having a specified hydroxyl value and a specified starter substance which may be used to produce closed-celled rigid polyurethane foams. Claim 13 claims a hydroxy value of 100 to 600 mg KOH/g and a starter selected from polyfunctional alcohol, sugar alcohols, aliphatic amines and aliphatic amines. Claim 14 recites a hydroxy value of 140 to 240 mg KOH/g and a starter of tolylenediamine. Claim 15 recites a hydroxy value of 140 to 240 mg KOH/g and a starter of trimethylolpropane.

The rejections of claims of claims 13 and 19 under 35 U.S.C. §102(b) over Heyman et al. U.S. 5,919,972 and of claims 14-15 under 35 U.S.C. §103(a) over Heyman et al. U.S.

5,919,972 in view of EP 786,480 and Isobe et al., U.S. 6,433,033 are respectfully traversed. In addition the rejections of claims of claims 13 and 19 under 35 U.S.C. §102(b) over Perry et al., U.S. 6,127,443 and of claims 14-15 under 35 U.S.C. §103(a) of Perry in view of Isobe et al., U.S. 6,433,033 are respectfully traversed.

None of the cited references discloses the claimed hydroxy value with the claimed starter substance.

Claim 13

This embodiment is directed to a graft polyol having a hydroxy value of 100 to 600 mg KOH/g and a starter selected from polyfunctional alcohol, sugar alcohols, aliphatic amines and aliphatic amines.

Neither Heyman et al. nor Perry describe a graft polyol having the claimed hydroxy value and a starter selected from polyfunctional alcohol, sugar alcohols, aliphatic amines and aliphatic amines.

Heyman et al. fail to describe a hydroxy value for the graft polyol component. As such this reference can not render a graft polyol having ;a hydroxy value of 100 to 600 mg KOH/g to be obvious. In the absence of a specific disclose of this claim limitation, the rejection based on obviousness can not be sustained and the decision of the examiner must be reversed.

Perry et al. fail to describe a graft polyol having a hydroxy number as claimed and a starter as claimed.

Perry et al describes a bicompositional polyol having different molecular weights and/or functionalities. (column 3, lines 34-36) The first polyol component fails to recite a

hydroxy number (column 3, line 58 through column 4, line 63) and as such can not render obvious the claimed graft polyol having a recited hydroxy number. The second polyol component may have a hydroxy number of from 160 to 800 but fails to suggest such a polyol in which the starter is polyfunctional alcohol, sugar alcohol, aliphatic amine or aliphatic amine (column 4, line 64 through column 5, line 10).

The basic deficiencies of the primary references are not cured by the secondary reference.

Isobe et al. has been cited for a disclosure of starter molecules, however fails to suggest the claimed hydroxy values, a deficiency in Heyman et al. and Perry et al. with the starter compounds as claimed.

The combination of Heyman et al. with EP '490 has not been applied to either of claims 13 or 19 and accordingly the combination fails to render claims 13 or 19 obvious.

As the references fail to identify the claimed starter compounds with the claimed hydroxy value the graft polyol of claim 13 is neither anticipated nor rendered obvious by these references. The decision of the examiner must be reversed.

Claim 14

This embodiment is directed to a graft polyol having a hydroxy value of 140 to 240 mg KOH/g and a starter of tolylenediamine.

Heyman et al. fail to describe a hydroxy value for the graft polyol component. As such this reference can not render a graft polyol having ;a hydroxy value of 140 to 240 mg KOH/g to

be obvious. In the absence of a specific disclosure of this claim limitation, the rejection can not be sustained. The decision of the examiner must be reversed.

Perry et al. fail to identify a starter compound of tolylenediamine.

The basic deficiencies of the primary references are not cured by the secondary reference.

Isobe et al. has been cited for a disclosure of starter molecules, however fails to suggest the claimed hydroxy values, a deficiency in Heyman et al. and Perry et al. with the starter compounds as claimed.

The combination of Heyman et al. with EP '490 has not been applied to claim 14 and accordingly the combination fails to render claim 14 obvious.

As the references fail to identify the claimed starter compounds with the claimed hydroxy value the graft polyol of claim 14 is not rendered obvious by these references and the decision of the examiner must be reversed.

Claim 15

This embodiment is directed to a graft polyol having a hydroxy value of 140 to 240 mg KOH/g and a starter of trimethylolpropane.

Heyman et al. fail to describe a hydroxy value for the graft polyol component. As such this reference can not render a graft polyol having a hydroxy value of 140 to 240 mg KOH/g to be obvious. In the absence of a specific disclosure of this claim limitation, the rejection based on obviousness must be withdrawn.

Perry et al. fail to identify a starter compound of trimethylolpropane.

The basic deficiencies of the primary references are not cured by the secondary reference.

Isobe et al. has been cited for a disclosure of starter molecules, however fails to suggest the claimed hydroxy values, a deficiency in Heyman et al. and Perry et al. with the starter compounds as claimed.

The combination of Heyman et al. with EP '490 has not been applied to claim 15 and accordingly the combination fails to render claim 15 obvious.

As the references fail to identify the claimed starter compounds with the claimed hydroxy value the graft polyol of claim 15 is not rendered obvious by these references. The decision of the examiner must be reversed.

In view of the errors committed by the examiner, his conclusions of obviousness are in error and must be reversed.

Respectfully submitted,

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(viii) Claims Appendix

Claim 1 A process for producing closed-celled rigid polyurethane foams by reacting

- a) crude MDI having an NCO content of from 29 to 33% by weight and a viscosity at 25°C in the range from 150 to 1000 mPa•s with
- b) compounds having at least two hydrogen atoms reactive toward isocyanate groups, in the presence of
- c) catalysts, and
- d) blowing agents,

which comprises the presence, among the compounds having at least two hydrogen atoms reactive toward isocyanate groups, of at least one graft polyol, wherein said closed-celled rigid polyurethane has a proportion of closed cells in the foam of at least 88%.

Claim 2 (previously presented): A process as claimed in claim 1, wherein the amount used of the graft polyol is up to 100% by weight, based on component b.

Claim 3: A process as claimed in claim 1, wherein the amount used of the graft polyol is from 0.5 to 70% by weight, based in each case on component b.

Claim 4 A process as claimed in claim 1, wherein the amount used of the graft polyol during the production of rigid polyurethane foams for use in refrigeration equipment is from 3 to 70% by weight, based on component b.

Claim 5 A process as claimed in claim 1, wherein the amount used of the graft polyol during the production of rigid polyurethane foams for use in sandwich components is from 0.5 to 35% by weight, based on component b.

Claim 6 A process as claimed in claim 1, wherein the graft polyol has a hydroxy value in the range from 20 to 210 mg KOH/g.

Claim 7 A process as claimed in claim 1, wherein the graft polyol particle distribution has a maximum at from 0.1 to 8 μm .

Claim 8 A process as claimed in claim 1, wherein the graft polyol has a bimodal particle size distribution.

Claim 9 A process as claimed in claim 1, wherein the graft polyol is prepared by in-situ polymerization of ethylenically unsaturated monomers in polyether alcohols having a functionality of from 2 to 8 and having a hydroxy value in the range from 100 to 800 mg KOH/g, obtained by an addition reaction of alkylene oxides onto H-functional starter

substances, the starter substances having been selected from the group consisting of polyfunctional alcohols, sugar alcohols, aliphatic amines, and aromatic amines.

Claim 10 A process as claimed in claim 1 wherein the graft polyol is prepared by in-situ polymerization of ethylenically unsaturated monomers in polyether alcohols which are obtained by an addition reaction of alkylene oxides onto tolylenediamine, using basic catalysis.

Claim 11 A process as claimed in claim 1, wherein the graft polyol is prepared by in-situ polymerization of ethylenically unsaturated monomers in polyether alcohols which are obtained by an addition reaction of alkylene oxides onto trimethylolpropane, using basic catalysis or catalysis by multimetal cyanide complexes.

Claim 12 A rigid polyurethane foam produced by the process of claim 1.

Claim 13 A graft polyol comprising polymerized ethylenically unsaturated monomers in polyether alcohols having a hydroxy value in the range from 100 to 600 mg KOH/g, obtained by an addition reaction of alkylene oxides onto H-functional starter substances, the starter substances having been selected from the group consisting of polyfunctional alcohols, sugar alcohols, aliphatic amines, and aromatic amines.

Claim 14 A graft polyol as claimed in claim 13, prepared by in-situ polymerization of ethylenically unsaturated monomers in polyether alcohols having a hydroxy value in the range from 140 to 240 mg KOH/g, which are obtained by an addition reaction of alkylene oxides onto tolylenediamine.

Claim 15 A graft polyol as claimed in claim 13, prepared by in-situ polymerization of ethylenically unsaturated monomers in polyether alcohols having a hydroxy value in the range from 140 to 240 mg KOH/g, which are obtained by an addition reaction of alkylene oxides onto trimethylolpropane.

Claim 17. The process of claim 1, wherein said closed-celled rigid polyurethane has a proportion of closed cells in the foam of at least 95%.

Claim 18. The process of claim 1, wherein said graft polyol is prepared via in-situ polymerization of ethylenically unsaturated monomers in polyether alcohol.

Claim 19 The graft polyol of claim 13, wherein said graft polyol is prepared via in-situ polymerization of ethylenically unsaturated monomers in polyether alcohol.

Application No. 10/478,694
Appeal of Office Action of December 7, 2007

(ix) Evidence Appendix

Gallager U.S. 5,208,271



US005208271A

United States Patent [19]
Gallagher

[11] **Patent Number:** **5,208,271**
[45] **Date of Patent:** **May 4, 1993**

[54] **FLEXIBLE POLYURETHANE FOAMS WITH
REDUCED TENDENCY FOR SHRINKAGE**

[75] **Inventor:** **James A. Gallagher**, Grosse Ile,
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[73] **Assignee:** **BASF Corporation**, Parsippany, N.J.

[21] **Appl. No.:** **970,448**

[22] **Filed:** **Nov. 2, 1992**

[51] **Int. Cl.³** **C09K 3/00**

[52] **U.S. Cl.** **521/174; 252/182.24;
252/182.25; 252/182.27; 521/176**

[58] **Field of Search** **252/182.24, 182.25,
252/182.27; 521/174, 176**

[56] **References Cited**

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4,026,845 5/1977 Kim et al. 260/2.5 S
4,101,468 7/1978 Perrey et al. 521/115

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OTHER PUBLICATIONS

D. R. Battice & W. J. Lopes, "New Cell Opening Sur-
factants for Molded High Resiliency Polyurethane
Foam," Oct. 1986, pp. 145-148.

Primary Examiner—Morton Foelak

Attorney, Agent, or Firm—Dennis V. Carmen

[57] **ABSTRACT**

A perfluorinated sulfonamide surfactant is provided
which reduces polyurethane foam shrinkage upon de-
molding. The surfactant is particularly useful to reduce
shrinkage of water-blown flexible polyurethane foams
without the need for mechanical crushing.

10 Claims, No Drawings

FLEXIBLE POLYURETHANE FOAMS WITH REDUCED TENDENCY FOR SHRINKAGE

1. FIELD OF THE INVENTION

The present invention is related to water-blown flexible polyurethane foams having a reduced tendency to shrink, more particularly to water-blown flexible polyurethane foams containing as a surfactant a perfluorinated sulfonamide.

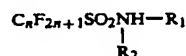
2. BACKGROUND OF THE INVENTION

To obtain a flexible foam adequately stabilized against collapse and having a good closed-cell structure, it is known to add a surfactant. A flexible foam having a high number of closed cells, however, leads to shrinkage. One means generally employed to open the cells and eliminate foam shrinkage is to mechanically treat the foam by crushing with rollers, with a vacuum technique, or by lancing. It would be desirable, however, to produce a surfactant that stabilizes the foam against collapse while opening the cells of the foam without the necessity for mechanical treatment.

The elimination of foam shrinkage by opening the cells using new types of surfactants was the topic of a paper by D. R. Battice, et al., *New Cell Opening Surfactants For Molded High Resiliency Polyurethane Foam*, 30th Annual Polyurethane Technical Marketing Conference, Oct. 15-17, 1986, pp. 145-148. The new surfactants that promoted good cell drainage and eliminated foam shrinkage were identified as X2-5249 and X2-5256, both silicone-based and manufactured at the time by Dow Corning. These surfactants successfully reduced foam shrinkage over a previous Dow Corning® 5043 surfactant.

3. SUMMARY OF THE INVENTION

It is an object of the invention to provide an alternate surfactant which reduces or eliminates shrinkage of flexible polyurethane foams, including the integral skin foams. This object is achieved by employing as a surfactant a perfluorinated sulfonamide compound represented by the following general formula:



wherein R₁ and R₂ are each independently hydrogen or a branched or unbranched alkyl, aryl, or aralkyl having 1-20 carbon atoms; with R₁ and R₂ optionally being bonded end to end as a heterocyclic ring; and R₁ and R₂ optionally containing internal to a carbon chain the groups —NR', —NR'₂, —O—, —SO₂—, —COO—, —OOC—, —CO—, —CONR—, —NR—CO—, or —SO₂NR', and/or preferably with at least one of R₁ or R₂ terminated with —OH, —COOH, —NH₂, —NHR', or —COH, wherein R' is independently a branched or unbranched alkyl having up to 18 carbon atoms, and n is from four (4) to twenty (20).

A preferred subgenus is R₁ and R₂ each independently comprising a branched or unbranched alkyl having from 1 and 8 carbon atoms, and independently terminated with a hydroxyl group, with n being from 6 to 10. A more preferred species is N-ethyl-N-2-hydroxyethyl perfluoro octane sulfonamide.

It has been found that perfluoro sulfonamide surfactants used in the invention prevent shrinkage of molded

flexible polyurethane foams, avoiding the necessity for mechanical crushing, and provide suitable alternatives to silicone-based surfactants. Suitable amounts of the surfactant are the minimum necessary to stabilize the foam against collapse while preventing shrinkage. Illustrative amounts range from 0.1 pbw to 5 pbw based on 100 pbw of polyol, preferably from 1.0 pbw to 2.5 pbw.

Methods of forming the sulfonamides are known and generally described in U.S. Pat. No. 4,101,468, incorporated herein by reference. For example, a fluorinated alkyl sulphochloride may be reacted with an amine to yield the corresponding fluorinated alkyl sulfonamide.

The organic polyisocyanates may include all essentially known aliphatic, cycloaliphatic, araliphatic, and preferably aromatic polyhydric isocyanates. Specific examples include: alkylene diisocyanates with 4 to 12 carbons in the alkylene group such as dodecane 1,12-diisocyanate, 2-ethyltetramethylene-1,4-diisocyanate, 2-methylpentamethylene-1,5-diisocyanate, tetramethylene-1,4-diisocyanate and preferably hexamethylene-1,6-diisocyanate; cycloaliphatic diisocyanates such as cyclohexane-1,3- and 1,4-diisocyanate as well as any mixtures of these isomers, 1-isocyanato-3,3,5-trimethyl-t-isocyanatomethylcyclohexane (isophorone diisocyanate), hexahydrotoluene-2,4- and 2,6-diisocyanate as well as the corresponding isomer mixtures, dicyclohexylmethane-4,4', 2,2'-, and 2,4'-diisocyanate as well as the corresponding isomer mixtures and preferably aromatic diisocyanates and polyisocyanates such as toluene-2,4- and 2,6-diisocyanate and the corresponding isomer mixtures, diphenylmethane-4,4', 2,4'-, and 2,2'-diisocyanate and the corresponding isomer mixtures, mixtures of diphenylmethane 4,4'- and 2,4'-diisocyanates, polyphenyl-polymethylene polyisocyanates, mixtures of diphenylmethane-4,4', 2,4', and 2,2'-diisocyanates and polyphenylpolymethylene polyisocyanates (crude MDI) as well as mixtures of crude MDI and toluene diisocyanates can be used individually or in the form of mixtures.

Frequently, so-called modified polyhydric isocyanates, i.e., products obtained by chemical reaction of organic diisocyanates and/or polyisocyanates are used. Examples include diisocyanates and/or polyisocyanates containing ester groups, urea groups, biuret groups, allophanate groups, carbodiimide groups, isocyanurate groups, uretdione groups, and/or urethane groups. Specific examples include organic, preferably aromatic polyisocyanates containing urethane groups and having an NCO content of 33.6 to 15 weight percent, preferably 31 to 21 weight percent, based on the total weight, e.g., with low molecular diols, triols, dialkylene glycols, trialkylene glycols or polyoxyalkylene glycols with a molecular weight of up to 800, modified diphenylmethane 4,4'-diisocyanate or toluene 2,4- and 2,6-diisocyanate, where examples of di- and polyoxyalkylene glycols that may be used individually or as mixtures include diethylene glycol, dipropylene glycol, polyoxyethylene glycol, polyoxypropylene glycol and polyoxypropylene polyoxyethylene glycols. Prepolymers containing NCO groups with an NCO content of 25 to 3.5 weight percent, preferably 21 to 14 weight percent, based on the total weight and produced from the polyester polyols and/or preferably polyether polyols described below and diphenylmethane 4,4'-diisocyanate, mixtures of diphenylmethane-2,4'- and 4,4'-diisocyanate, toluene-2,4- and/or 2,6-diisocyanates or crude MDI are also suitable. Furthermore, liquid polyisocya-

nates containing carbodiimide groups and/or isocyanurate rings and having an NCO content of 33.6 to 15 weight percent, preferably 31 to 21 weight percent, based on the total weight, are also suitable, e.g., based on diphenylmethane 4,4', 2,4', and/or 2,2'-diisocyanate and/or toluene 2,4- and/or 2,6-diisocyanate.

The modified polyisocyanates may optionally be mixed together or mixed with unmodified organic polyisocyanates such as diphenylmethane 2,4'- and 4,4'-diisocyanate, crude MDI, toluene 2,4'- and/or 2,6-diisocyanate.

The following have proven especially successful as organic polyisocyanates and are preferred for use in the production of flexible polyurethane foams: prepolymers containing NCO groups and having an NCO content of 9 to 25 weight percent, especially those based on polyether polyols and one or more diphenylmethane diisocyanate isomers, preferably diphenylmethane 4,4'-diisocyanate, and/or modified organic polyisocyanates containing urethane groups and having an NCO content of 15 to 33.6 weight percent, especially those based on diphenylmethane 4,4'-diisocyanate or diphenylmethane diisocyanate isomer mixtures; mixtures of toluene 2,4- and 2,6-diisocyanates, mixtures of toluene diisocyanates and crude MDI or especially mixtures of the aforementioned prepolymers based on diphenylmethane diisocyanate isomers and crude MDI.

Preferred high molecular compounds having at least two reactive hydrogens include those with a functionality of 2 to 8, preferably 2 to 6, and a molecular weight of 400 to 8,000, preferably 1,200 to 6,000. For example, polyether polyamines and/or preferably polyols selected from the group of polyether polyols, polyester polyols, polythioether polyols, polyester amides, polyacetals containing hydroxyl groups and aliphatic polycarbonates containing hydroxyl groups or mixtures of at least two of the aforementioned polyols have proven suitable. Polyester polyols and/or polyether polyols are preferred.

Suitable polyester polyols can be produced, for example, from organic dicarboxylic acids with 2 to 12 carbons, preferably aliphatic dicarboxylic acids with 4 to 6 carbons, and polyhydric alcohols, preferably diols, with 2 to 12 carbons, preferably 2 to 6 carbons. Examples of dicarboxylic acids include succinic acid, glutaric acid, adipic acid, suberic acid, azelaic acid, sebacic acid, decanedicarboxylic acid, maleic acid, fumaric acid, phthalic acid, isophthalic acid, and terephthalic acid. The dicarboxylic acids can be used individually or in mixture. Instead of the free dicarboxylic acids, the corresponding dicarboxylic acid derivatives may also be used as dicarboxylic acid esters of alcohols with 1 to 4 carbons or dicarboxylic acid anhydrides. Dicarboxylic acid mixtures of succinic acid, glutaric acid and adipic acid in quantity ratios or 20-35:35-50:20-32 parts by weight are preferred, especially adipic acid. Examples of dihydric and polyhydric alcohols, especially diols, include ethanediol, diethylene glycol, 1,2- and 1,3-propanediol, dipropylene glycol, 1,4-butanediol, 1,5-pentanediol, 1,6-hexanediol, 1,10-decanediol, glycerol, and trimethylolpropane. Ethanediol, diethylene glycol, 1,4-butanediol, 1,5-pentanediol, 1,6-hexanediol, or mixtures of at least two of these diols are preferred, especially mixtures of 1,4-butanediol, 1,5-pentanediol, and 1,6-hexanediol. Furthermore, polyester polyols of lactones, e.g., ϵ -caprolactone or hydroxycarboxylic acids, e.g., δ -hydroxycaproic acid, may also be used.

The polyester polyols can be produced by polycondensation or organic polycarboxylic acids, e.g., aromatic or preferably aliphatic polycarboxylic acids and/or derivatives thereof and polyhydric alcohols in the absence of catalysts or preferably in the presence of esterification catalysts, preferably in an atmosphere of inert gases, e.g., nitrogen, carbon monoxide, helium, argon, etc., in the melt at temperatures of 150° to 250° C., preferably 180° to 220° C., optionally under reduced pressure up to the desired acid value, which is preferably less than 10, especially less than 2. In a preferred version, the esterification mixture is subjected to polycondensation at the temperatures mentioned above up to an acid value of 80 to 30, preferably 40 to 30, under normal pressure and then under a pressure of less than 500 mbar, preferably 50 to 150 mbar. Examples of suitable esterification catalysts include iron, cadmium, cobalt, lead, zinc, antimony, magnesium, titanium, and tin catalysts in the form of metals, metal oxides, or metal salts. However, polycondensation may also be performed in liquid phase in the presence of solvents and/or entraining agents such as benzene, toluene, xylene, or chlorobenzene for azeotropic distillation of the water of condensation.

To produce the polyester polyols, the organic polycarboxylic acids and/or derivatives thereof and polyhydric alcohols are preferably polycondensed in a molar ratio of 1:1-1.8, preferably 1:1.05-1.2.

The resultant polyester polyols preferably have a functionality of 2 to 4, especially 2 to 3, and a molecular weight of 480 to 3,000, preferably 1,200 to 3,000, and especially 1,800 to 2,500.

However, polyether polyols, which can be obtained by known methods, are especially preferred for use as the polyols. For example, polyether polyols can be produced by anionic polymerization with alkali hydroxides such as sodium hydroxide or potassium hydroxide or alkali alcoholates such as sodium methylate, sodium ethylate, or potassium ethylate or potassium isopropylate as catalysts and with the addition of at least one initiator molecule containing 2 to 8, preferably 2 to 6, reactive hydrogens or by cationic polymerization with Lewis acids such as antimony pentachloride, boron trifluoride etherate, etc., or bleaching earth as catalysts from one or more alkylene oxides with 2 to 4 carbons in the alkylene group.

Suitable alkylene oxides include, for example, tetrahydrofuran, 1,3-propylene oxide, 1,2- and 2,3-butylene oxide, styrene oxide and preferably ethylene oxide and 1,2-propylene oxide. The alkylene oxides may be used individually, in alternation one after the other, or as a mixture. Examples of suitable initiator molecules include water, organic dicarboxylic acids such as succinic acid, adipic acid, phthalic acid and terephthalic acid, aliphatic and aromatic, optionally N-mono, N,N- and N,N'-dialkyl substituted diamines with 1 to 4 carbons in the alkyl group such as optionally mono- and dialkyl-substituted ethylenediamine, diethylenetriamine, triethylenetetramine, 1,3-propylenediamine, 1,3- and 1,4-butylenediamine, 1,2-, 1,3-, 1,4-, 1,5-, and 1,6-hexamethylenediamine, phenylenediamines, 2,3- 2,4-, and 2,6-toluenediamine, and 4,4-, 2,4'-, and 2,2'-diaminodiphenylmethane.

Suitable initiator molecules also include alkanolamines such as ethanolamine, diethanolamine, N-methyl- and N-ethylethanolamine, N-methyl- and N-ethyldiethanolamine and triethanolamine plus ammonia. Suitable polyhydric alcohols include ethanediol, 1,2-

propanediol and 1,3-propanediol, diethylene glycol, dipropylene glycol, 1,4-butanediol, 1,6-hexanediol, glycerol, trimethylolpropane, pentaerythritol, sorbitol, and sucrose, although preferred for flexible foam formation are the dihydric and trihydric alcohols.

The polyether polyols, preferably polyoxypropylene polyols and polyoxypropylene-polyoxyethylene-polyols having a functionality of preferably 2 to 6 and especially 2 to 4 and have a molecular weight of 400 to 8,000, preferably 1,200 to 6,000 and especially 1,800 to 4,000, and suitable polyoxytetramethylene glycols have a molecular weight up to about 3,500.

Suitable polyether polyols also include polymer modified polyether polyols, preferably graft polyether polyols, especially those based on styrene and/or acrylonitrile, which are produced by in situ polymerization of acrylonitrile, styrene or preferably mixtures of styrene and acrylonitrile, e.g., in a weight ratio of 90:10 to 10:90, preferably 70:30 to 30:70, preferably in the aforementioned polyether polyols according to the procedures described in German Patent Nos. 1,111,394; 1,222,669 (U.S. Pat. Nos. 3,304,273; 3,383,351; 3,523,093); 1,152,536 (British Patent No. 1,040,452); and 1,152,537 (British Patent No. 987,618); as well as polyether polyol dispersions containing as the disperse phase, usually in the amount of 1 to 50 weight percent, preferably 2 to 25 weight percent, e.g., polyureas, polyhydrazides, polyurethanes containing tertiary amino groups and/or melamine and described, for example, in European Patent No. B 11,752 (U.S. Pat. No. 4,304,708), U.S. Pat. No. 4,374,209 and German Patent No. A 3,231,497.

Like the polyester polyols, the polyether polyols may be used either individually or in the form of mixtures. Furthermore, they can be mixed with the graft polyether polyols or polyester polyols as well as the polyester amides containing hydroxyl groups, the polyacetals, polycarbonates, and/or polyether polyamines.

Examples of hydroxyl group-containing polyacetals that can be used include, for example, the compounds that can be produced from glycols such as diethylene glycol, triethylene glycol, 4,4'-dihydroxyethoxydiphenyldimethylmethane, hexanediol and formaldehyde. Suitable polyacetals can also be produced by polymerization of cyclic acetals.

Suitable hydroxyl group-containing polycarbonates include those of the known type such as those obtained by reaction of diols, e.g., 1,3-propanediol, 1,4-butanediol, and/or 1,6-hexanediol, diethylene glycol, triethylene glycol or tetraethylene glycol with diaryl carbonates, e.g., diphenyl carbonate, or phosgene.

The polyester amides include the mainly linear condensates obtained from polyvalent saturated and/or unsaturated carboxylic acids and their anhydrides and polyhydric saturated and/or unsaturated amino alcohols or mixtures of polyhydric alcohols and amino alcohols and/or polyamines.

Suitable polyether polyamines can be produced from the polyether polyols mentioned above by known methods. Examples include cyanoalkylation of polyoxalkylene polyols and subsequent hydrogenation of the nitrile thus formed (U.S. Pat. No. 3,267,050) or partial or complete amination or polyoxalkylene polyols with amines or ammonia in the presence of hydrogen and catalysts (German Patent No. 1,215,373).

The flexible foam of the invention can be produced with or without the use of chain extenders and/or crosslinking agents. To modify the mechanical properties,

e.g., hardness, however, it has proven advantageous to add chain extenders, crosslinking agents, or optionally even mixtures thereof. Suitable chain extenders and/or crosslinking agents include diols and/or triols with a molecular weight of less than 400, preferably 60 to 300. Examples include aliphatic, cycloaliphatic and/or araliphatic diols with 2 to 14 carbons, preferably 4 to 10 carbons, such as ethylene glycol, 1,3-propanediol, 1,10-decanediol, o-, m-, and p-dihydroxycyclohexane, diethylene glycol, dipropylene glycol, and preferably 1,4-butanediol, 1,6-hexanediol and bis(2-hydroxyethyl)hydroquinone, triols such as 1,2,4- and 1,3,5-trihydroxycyclohexane, glycerol and trimethylolpropane and low molecular hydroxyl group-containing polyalkylene oxides based on ethylene oxide and/or 1,2-propylene oxide and the aforementioned diols and/or triols as initiator molecules.

In addition to the aforementioned diols and/or triols, or in mixture with them as chain extenders or crosslinking agents to produce the cellular polyurethane-polyurea elastomers according to this invention, it is also possible to use secondary aromatic diamines, primary aromatic diamines, 3,3'-di- and/or 3,3',5,5'-tetraalkyl-substituted diaminodiphenylmethanes.

Blowing agents that can be used according to this invention include low boiling fluorinated compounds that have little or no solubility in the isocyanate, polyether, or polyester selected from the group of fluorinated or perfluorinated hydrocarbons, perfluorinated ethers, as well as sulfur hexafluoride, chlorofluorocarbons, or water. Preferably, the flexible foams are all water blown although within the scope of the invention are mixtures of water and fluorocarbons or other blowing agents having an ozone depleting potential of less than 0.05. The amount of water used as a blowing agent ranges from 0.5 pbw to 4 pbw based on 100 pbw of the polyol.

Suitable catalysts for producing the cellular plastics according to the polyisocyanate polyaddition process include especially compounds that greatly accelerate the reaction of the hydroxyl group containing compounds of polyol component and optionally with the organic optionally modified polyisocyanates (a). Examples include organic metal compounds, preferably tin compounds such as tin (II) salts of organic carboxylic acids, e.g., tin (II) acetate, tin (II) octoate, tin (II) ethylhexoate and tin (II) laurate, as well as the dialkyltin (IV) salts of organic carboxylic acids, e.g., dibutyltin diacetate, dibutyltin dilaurate, dibutyltin maleate, and diocetyl tin diacetate. The organic metal compounds are used alone or preferably in combination with strong basic amines. Examples include amidines such as 2,3-dimethyl-3,4,5,6-tetrahydropyrimidine, tertiary amines such as triethylamine, tributylamine, dimethylbenzylamine, N-methylmorpholine, N-ethylmorpholine, N-cyclohexylmorpholine, N,N,N',N'-tetramethylethylenediamine, N,N,N',N'-tetramethylbutanediamine, pentamethyldiethylenetriamine, tetramethyldiaminoethyl ester, bis(dimethylaminopropyl)urea, dimethylpiperazine, 1,2-dimethylimidazole, 1-azabicyclo[2.2.0]octane and preferably 1,4-diazabicyclo[2.2.2]octane and alkanolamine compounds such as triethanolamine, triisopropanolamine, N-methyl- and N-ethyldiethanolamine and dimethylethanolamine.

Suitable catalyst also include tris(dialkylamino)-s-hexahydrotriazines, especially tris(N,N-dimethylaminopropyl)-s-hexahydrotriazine, tetraalkylammonium hydroxides such as tetramethylammonium hydroxide,

alkali hydroxides such as sodium hydroxide and alkali alcoholates such as sodium methylate and potassium isopropylate as well as alkali salts of long-chain fatty acids with 10 to 20 carbons and optionally OH side groups. A 0.001 to 5 weight percent, especially 0.05 to 2 weight percent, catalyst or catalyst combination based on the weight of polyol component is preferred.

Optionally, other additives and/or processing aids (f) may be incorporated into the reaction mixture to produce the cellular plastics by the polyisocyanate polyaddition process. Examples include surface active substances, fillers, dyes, pigments, flame retardants, hydrolysis preventing agents, fungistatic and bacteriostatic agents.

Examples of surface active substances include compounds that support the homogenization of the starting materials such as the sodium salts of castor oil sulfates or of fatty acids as well as salts of fatty acids with amines, e.g., diethylamine oleate, diethanolamine stearate, diethanolamine ricinoleate, salts of sulfonic acid, e.g., alkali or ammonium salts of dodecylbenzenesulfonic acid or dinaphthylmethanedisulfonic acid and ricinoleic acid. Other foam stabilizers that can be admitted include siloxaneoxyalkylene copolymers and other organopolysiloxanes, ethoxylated alkylphenols, ethoxylated fatty alcohols, paraffin oils, castor oil and ricinoleic acid esters, Turkey red oil, and peanut oil as well as cell regulators such as paraffins, fatty alcohols and dimethyl polysiloxanes. Furthermore, the oligomeric acrylates with polyoxyalkylene and fluoroalkane side groups described above are also suitable for improving the emulsifying effect, the cell structure and/or for stabilizing the foam.

Fillers, especially reinforcing fillers, are understood to refer to the known conventional organic and inorganic fillers, reinforcing agents, weighing agents, agents to improve abrasion properties in paints, coating agents, etc. Specific examples include inorganic fillers such as silicate minerals, e.g., lamellar silicates such as antigorite, serpentine, hornblendes, amphiboles, chrysotile, talc; metal oxides such as kaolin, aluminum oxides, titanium oxides and iron oxides, metal salts such as chalk, heavy spar (barite) and inorganic pigments such as cadmium sulfide, zinc sulfide as well as glass, etc. Kaolin (China clay), aluminum silicate and co-precipitates of barium sulfate and aluminum silicate as well as natural and synthetic fibrous minerals such as wollastonite, metal fibers, and especially glass fibers of various lengths, optionally sized, are preferred. Examples of organic fillers include coal, melamine, colophony, cyclopentadienyl resins and graft polymers as well as cellulose fibers, nylon, polyacrylonitrile, polyurethane and polyester fibers based on aromatic and/or aliphatic dicarboxylic acid esters and especially carbon fibers.

The organic and inorganic fillers may be used individually or as mixtures and are incorporated into the reaction mixture in amounts of 0.5 to 50 weight percent, preferably 1 to 40 weight percent, based on the weight of the isocyanate, polyol, and optional chain extender components.

Suitable flame retardants include, for example, tris-cresyl phosphate, tris-2-chloroethyl phosphate, tris-chloropropyl phosphate and tris-2,3-dibromopropyl phosphate.

In addition to the aforementioned halogen substituted phosphates, inorganic flame retardants may also be used such as red phosphorus, aluminum oxide hydrate, antimony trioxide, arsenic oxide, aluminum polyphosphate

and calcium sulfate or cyanuric acid derivatives such as melamine or mixtures of at least two flame retardants, e.g., ammonium polyphosphates and a melamine plus optionally cornstarch for making the polyisocyanate polyaddition products flame resistant. In general, it has proven expedient to use 5 to 50 parts by weight, preferably 5 to 25 parts by weight, of the aforementioned flame retardants for each 100 parts by weight of the polyol component.

Details regarding the aforementioned other conventional additives and processing aids can be obtained from the technical literature, e.g., the monograph by J. H. Saunders and K. C. Frisch, "High Polymers," Volume XVI, *Polyurethanes*, Parts 1 and 2, Interscience Publishers, 1962 and 1964 or *Plastics Handbook, Polyurethanes*, Volume VII, Hanser-Verlag, Munich, Vienna, 1st and 2nd Editions, 1966 and 1983.

To produce the cellular plastics containing urea and/or preferably urethane groups, the organic polyisocyanates, high molecular polyol compounds with at least two reactive hydrogens and optional chain extenders and/or crosslinking agents are reacted in amounts such that the equivalent ratio of NCO groups of polyisocyanates to the total reactive hydrogens of the polyol component and optionally amounts to 1:0.85-1.25, preferably 1:0.95-1.15.

The cellular plastics of polyisocyanate polyaddition products, preferably cellular elastomers or especially flexible foams, are produced to advantage by the one-shot process, e.g., with the high pressure or low pressure technique using open or closed molds, e.g., metal molds.

The starting components are mixed at a temperature of 15° to 90° C., preferably 20° to 35° C., and are placed in an open mold or optionally in a closed mold under elevated pressure. The mixing can be performed mechanically by means of a stirrer or by means of a stirring screw or under a high pressure in the so-called counter-current injection method as mentioned above. The mold temperature should be 20° to 60° C., preferably 30° to 60° C., and especially 45° to 50° C.

The soft flexible foams produced by the process according to the invention as well as the corresponding integral foams have a density of 0.02 to 0.75 g/cm³, where the density of the foams is preferably 0.025 to 0.24 g/cm³ and especially 0.03 to 0.1 g/cm³ and the density of the integral foams is preferably 0.08 to 0.75 g/cm³, especially 0.24 to 0.6 g/cm³. The flexible foams and integral foams are used, for example, in the automobile industry, the aircraft industry and the shipbuilding industry, in the furniture and athletic equipment industry and as seating materials.

EXAMPLES

The invention will now be described by means of examples which are not limiting to the scope of the invention but merely illustrative of embodiments within its scope.

Polyol A

is a trimethylolpropane-initiated polyoxypropylene polyoxyethylene polyether polyol having 13 weight percent polyoxyethylene cap and a nominal hydroxyl number of about 35.

Polyol B

is a 30 weight percent of 1:1 acrylonitrile to styrene graft polyol having a nominal hydroxyl number of 24 in a trimethylolpropane-initiated propylene oxide-ethylene oxide adduct terminated with 13 weight

-continued

Polyol C	percent ethylene oxide. is a 31 weight percent 2:1 acrylonitrile styrene graft polyol in a 95:5 weight percent blend of a glycerine-initiated ethylene oxide/propylene oxide adduct terminated with 18.5 weight percent ethylene oxide and having a nominal hydroxyl number of 35, and glycerine, respectively.
Iso A	is an 80:20 blend of 2,4'-and 2,6'-isomers of toluene diisocyanate.
DEOA	is diethanolamine, a chain extender.
NIAx C-225	is a complex amine catalyst available from Union Carbide Corporation.
FOAMREZ UL-1	is an organotin catalyst available from WITCO Corp.
SURFACTANT 1	is DC-5043, a high resiliency silicone surfactant available from Air Products.
Surfactant 2	is X2-5249, an experimental surfactant from Dow Corning.
Surfactant 3	is 50 weight percent N-ethyl-N-2- hydroxyethyl-perfluoro octane sulfonamide in toluene.

Polyol A and C were, along with water, DEOA, NIAx C-225, a tin catalyst FOAMREZ, and Surfactant 3 were handmixed at 3,000 rpm for 30 seconds in the parts by weight shown below in Table 1, Sample 1. To the mixture was added ISO A in the amount shown, mixed for ten (10) seconds, and poured into a 2"×10"×10" mold. The sample was allowed to foam and subsequently tested for shrinkage. The foam blocks were not subject to crushing or mechanical treatment prior to measurement. To measure shrinkage, a ruler was placed from the highest point at each end of the molded foam block and traversing the deepest recession in the block, at which point the distance from the ruler to the deepest point in the recession was measured and is reported below as shrinkage.

Samples 2-6 were repeated using the above procedure but in the amounts and with the materials reported in the table below each sample.

TABLE 1

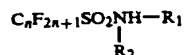
SAMPLE	1*	2	3*	4*	5	6
POLYOL A	60	60	58.2	58.2	58.2	58.2
POLYOL B	40	40	—	—	—	—
POLYOL C	—	—	41.8	41.8	41.8	41.8
WATER	4	4	4	4	4	4
DEOA	1.5	1.5	1.5	1.5	1.5	1.5
NIAx C-225	0.7	0.7	0.7	0.7	0.7	0.7
FOAMREZ	0.015	0.015	0.015	0.015	0.015	0.015
UL-1	—	—	—	—	—	—
SURFAC-	1.5	—	1.5	—	—	—
TANT 1	—	—	—	1.5	—	—
SURFAC-	—	1.5	—	—	1.5	1.0
TANT 2	—	—	—	—	—	—
SURFAC-	—	—	—	—	—	—
TANT 3	—	—	—	—	—	—
ISO A	47.2	47.2	51.3	51.3	51.3	51.3
SHRINK-	0.4	0.0	1.9	2.1	1.4	1.2
AGE	—	—	—	—	—	—

*COMPARATIVE EXAMPLES

The results indicate that a foam prepared with Surfactant 3 within the scope of the invention demonstrated little or no shrinkage. The surfactant of the present invention performed as well, if not better, than the foams prepared using convention Surfactants 1 and 2.

What I claim is:

1. A polyol composition comprising a polyoxyalkylene polyether polyol and a perfluorinated sulfonamide surfactant having the following formula:



wherein R₁ and R₂ are each independently hydrogen or a branched or unbranched alkyl, aryl, aralkyl having 1-20 carbon atoms; with R₁ and/or R₂ optionally being bonded end to end as a heterocyclic ring; and R₁ and/or R₂ optionally containing as internal to an alkyl chain the groups —NR'—, —NR'₂—, —O—, —SO₂—, —OOC—, —COO—, —CO—, —CONR'—, —NR—CO—, or —SO₂NR'; and/or as terminal to an alkyl chain the groups —OH, —COOH—, —NH₂, —NHR'¹, —COH, and R' is independently a branched or unbranched alkyl having up to 18 carbon atoms; and wherein n is from 4 to 20.

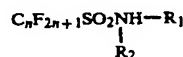
2. The polyol composition of claim 1, further containing water, a chain extender, and a polyurethane promoting catalyst.

3. The polyol composition of claim 1, wherein the amount of surfactant is from 1.0 to 5.0 parts by weight based on 100 parts by weight of polyol.

4. The polyol composition of claim 1, wherein R₁ and R₂ are each a branched or unbranched alkyl group.

5. The polyol composition of claim 4, wherein the surfactant is N-ethyl-N-2-hydroxyethyl perfluoro octane sulfonamide.

6. A process for the preparation of a polyol composition comprising blending a polyoxyalkylene polyether polyol and a perfluorinated sulfonamide surfactant having the following formula:



wherein R₁ and R₂ are each independently hydrogen or a branched or unbranched alkyl, aryl, aralkyl having 1-20 carbon atoms; with R₁ and/or R₂ optionally being bonded end to end as a heterocyclic ring; and R₁ and/or R₂ optionally containing as internal to an alkyl chain the groups —NR'—, —NR'₂—, —O—, —SO₂—, —OOC—, —COO—, —CO—, —CONR'—, —NR—CO—, or —SO₂NR'; and/or as terminal to an alkyl chain the groups —OH, —COOH—, —NH₂, —NHR'¹, —COH, and R' is independently a branched or unbranched alkyl having up to 18 carbon atoms; and wherein n is from 4 to 20.

7. The process of claim 6, further containing water, a chain extender, and a polyurethane promoting catalyst.

8. The process of claim 6, wherein the amount of surfactant is from 1.0 to 5.0 parts by weight based on 100 parts by weight of polyol.

9. The process of claim 6, wherein R₁ and R₂ are each a branched or unbranched alkyl group.

10. The process of claim 6, wherein the surfactant is N-ethyl-N-2-hydroxyethyl perfluoro octane sulfonamide.

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Application No. 10/478,694
Appeal of Office Action of December 7, 2007

(x) *Related Proceedings Appendix*

none